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9: Common Non-Equilibrium Calculations

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Why Non-Equilibrium MD (NEMD)?

- Classical Molecular Dynamics often used as a thermodynamic equilibrium technique
 - Newton's Equations + pairwise central forces conserve energy
 - At long times (depending on IC's and BC's) → Microcanonical Ensemble
- We are interested in non-equilibrium properties
 - Transport: rheology

$$\sigma = \eta \dot{\gamma}$$

- How to obtain?
 - Near equilibrium or fluctuations about equilibrium
 - Linear response regime
 - Effectively zero rate transport coefficients
 - Need long-time for good statistics
- What about far from equilibrium?
 - High rates, large gradients
 - General time dependent behavior

Non-Equilibrium Ensemble Averages

- Rheological observables – compute p_{xy} ,
fix ave/spatial
 - Stress and strain-rate (linear regime)
 - Irving-Kirkwood (1950) *J Chem Phys*, v. 18, p. 817

$$\sigma_{\alpha\beta} = \left\langle \frac{1}{V} \sum_{i=1}^N \left[\sum_{j \neq i} \frac{r_{ij}^{\alpha} f_{ij}^{\beta}}{2} + m_i (v_i^{\alpha} - u^{\alpha})(v_j^{\beta} - u^{\beta}) \right]; f^N(\mathbf{r}, \mathbf{p}, t) \right\rangle$$

$$\dot{\gamma} = \left[\nabla \left\langle \sum_{i=1}^N \mathbf{v}_i \delta(\mathbf{r}_i - \mathbf{r}) \right\rangle \right]_{\alpha\beta} = [\nabla \mathbf{u}(r)]_{\alpha\beta} \quad \frac{\sigma_{\alpha\beta}}{\dot{\gamma}} = \eta$$

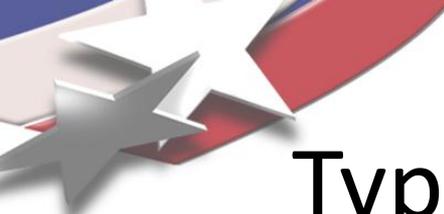
- Again, in practice these become time averages
- How long is long enough?



Non-Equilibrium Steady States

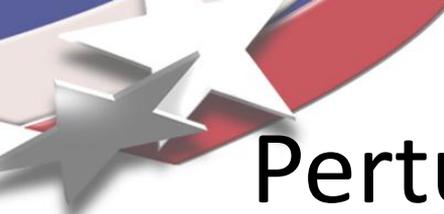
- What happens when a constant force (through boundary conditions – applied gradient, or external field) is applied to Equilibrium System following Newton's Equations for particle dynamics?
 - E.g., cause particles to flow
 - For pairwise central forces, Newton's Equations conserve energy
 - Constant force gives constant acceleration so kinetic energy (temperature) increases with time
- What to do for constant (steady-state) temperature?
 - Thermostat (on fluctuations about average) to balance energy input

- Section 6.16 of How to $k_B T = \frac{3(N-1)}{2} \left\langle \sum_i m_i (\mathbf{v}_i(t) - \mathbf{u}(r,t))^2 \right\rangle$



Typical NEMD Techniques (Rheology)

- Non-Hamiltonian Systems – “perturb” equations of motion
 - SLLOD + Parrinello-Rahman: shear flow
 - `fix nvt/sllod + fix deform`
- Boundary Modifications
 - Lees-Edwards
 - Steady Couette Flow
 - Muller-Plathe: shear or heat flow
 - `fix viscosity`
 - `fix thermal/conductivity`
 - Deletion and insertion
 - Mass flow



Perturbations to Equations of Motion

- General Approach

$$\dot{\mathbf{q}} = \mathbf{p} / m + \mathbf{A}_p(\mathbf{q}, \mathbf{p}) \cdot \mathcal{F}(t)$$

$$\dot{\mathbf{p}} = \mathbf{F} - \mathbf{A}_q(\mathbf{q}, \mathbf{p}) \cdot \mathcal{F}(t)$$

- Shear
- Heat flow

$$\dot{\mathbf{q}}_i = \mathbf{p}_i / m_i$$

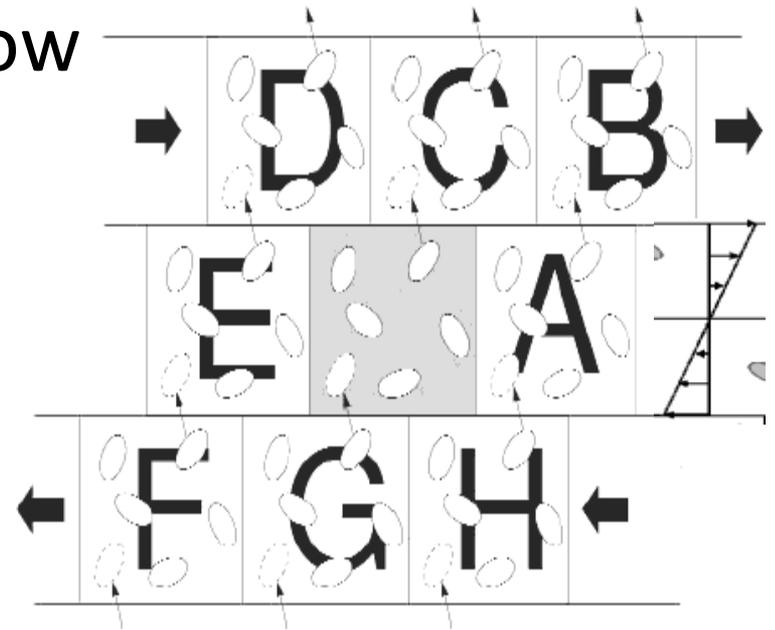
$$\dot{\mathbf{p}}_i = \mathbf{F}_i - \delta\varepsilon_i \mathcal{F}(t) + \frac{1}{2} \sum_j \mathbf{F}_{ij}(\mathbf{r}_{ij} \cdot \mathcal{F}(t)) - \frac{1}{2N} \sum_j \sum_k \mathbf{F}_{jk}(\mathbf{r}_{jk} \cdot \mathcal{F}(t))$$

- Diffusion

Allen and Tildesley, *Computer Simulation of Liquids*

Lees-Edwards Boundary Conditions

- Remap positions and velocities of particles crossing PBC
- Steady Shear (Couette) Flow
- Thermostat
 - E.g., Nose-Hoover
- No time dependent flow



Evans and Morris, *Statistical Mechanics of Nonequilibrium Liquids*

SLLOD + Parinello-Rahman

- Apply Shear Perturbation to each particle
 - Deform Box/particle positions

$$\dot{\mathbf{q}}_i = \mathbf{p}_i / m_i + \mathbf{q}_i \cdot \nabla \mathbf{u}$$

$$\dot{\mathbf{p}}_i = \mathbf{F}_i - \mathbf{p}_i \cdot \nabla \mathbf{u}$$

- Remap positions and/velocities across PBC
- Thermostat!
 - E.g., Nose-Hoover

- Profile biased vs. profile unbiased

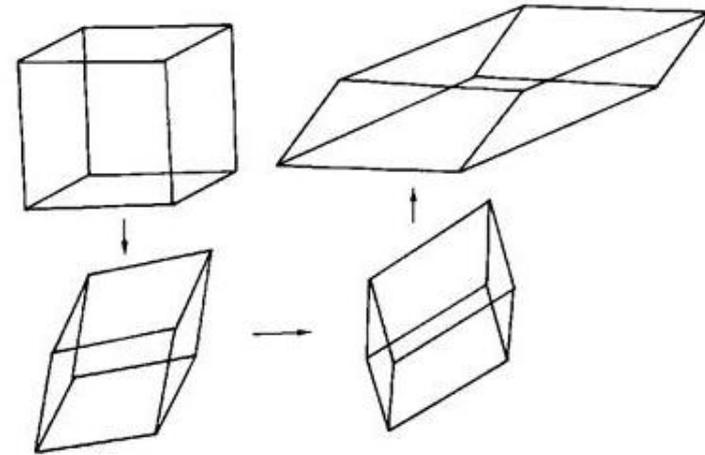
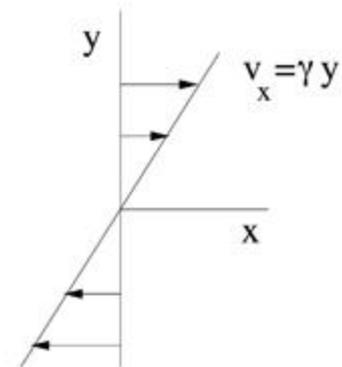
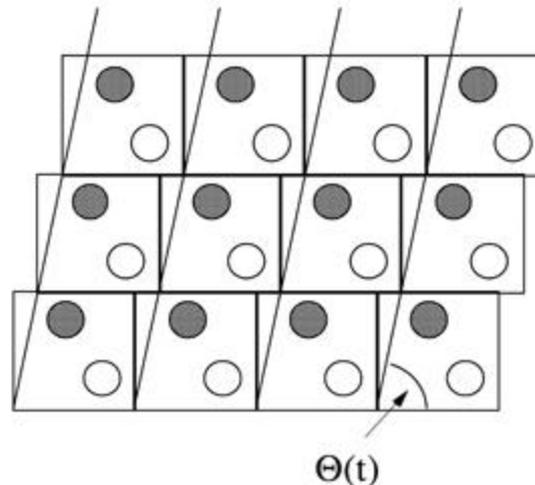


Fig. 7.3 Changing box-shape.

Evans and Morris, *Statistical Mechanics of Nonequilibrium Liquids*



$$\nabla \mathbf{u}(\mathbf{r}, t) = \begin{bmatrix} 0 & 0 \\ \gamma & 0 \end{bmatrix}$$

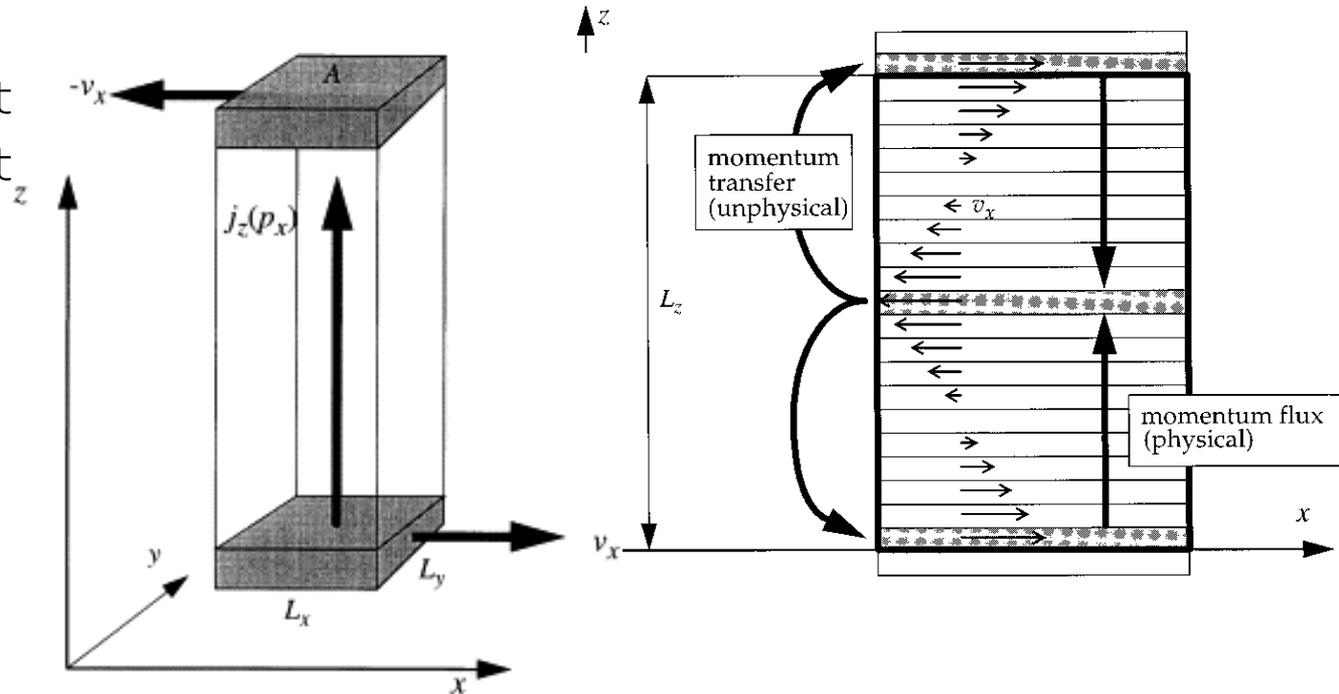
Muller-Plathe Approach

- Bin system in z
- Viscosity: swap opposed velocities in top and middle bins

- fix viscosity
- fix ave/spat

$$j_z(p_x) = -\eta \frac{\partial v_x}{\partial z}$$

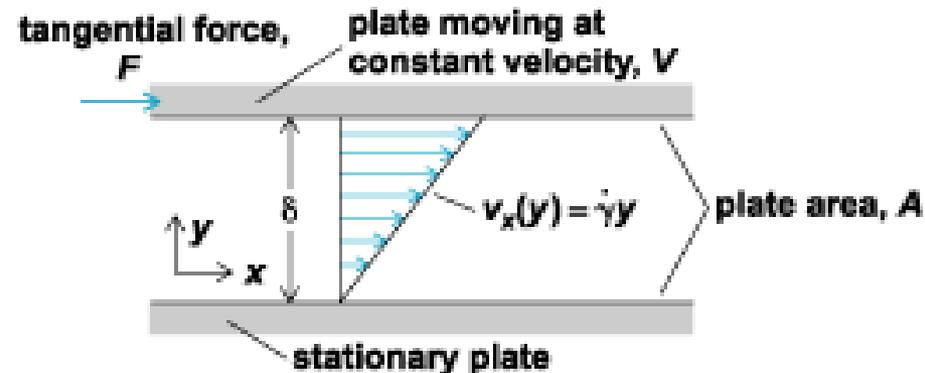
$$j_z(p_x) = \frac{P_{tot}}{2tL_x L_y}$$



- Can swap “hot” and “cold” (difference in squared velocity magnitude) atoms for thermal conductivities

Additional Rheology Relevant NE Simulations

- Initial and boundary conditions
 - Oscillatory
 - Large amplitude, high frequency
 - Failure, crazing
 - Phase changes
 - Concentration gradients
 - Dispersion stability
 - Evaporation
 - Shock



Rheology Applications

- What's possible?
- Practical issues
 - Long time averages – how long is long enough!
 - statistics